

This Page Is Inserted by IFW Operations
and is not a part of the Official Record

BEST AVAILABLE IMAGES

Defective images within this document are accurate representations of the original documents submitted by the applicant.

Defects in the images may include (but are not limited to):

- BLACK BORDERS
- TEXT CUT OFF AT TOP, BOTTOM OR SIDES
- FADED TEXT
- ILLEGIBLE TEXT
- SKEWED/SLANTED IMAGES
- COLORED PHOTOS
- BLACK OR VERY BLACK AND WHITE DARK PHOTOS
- GRAY SCALE DOCUMENTS

IMAGES ARE BEST AVAILABLE COPY.

As rescanning documents *will not* correct images,
please do not report the images to the
Image Problem Mailbox.

PCT

WORLD INTELLECTUAL PROPERTY ORGANIZATION
International Bureau

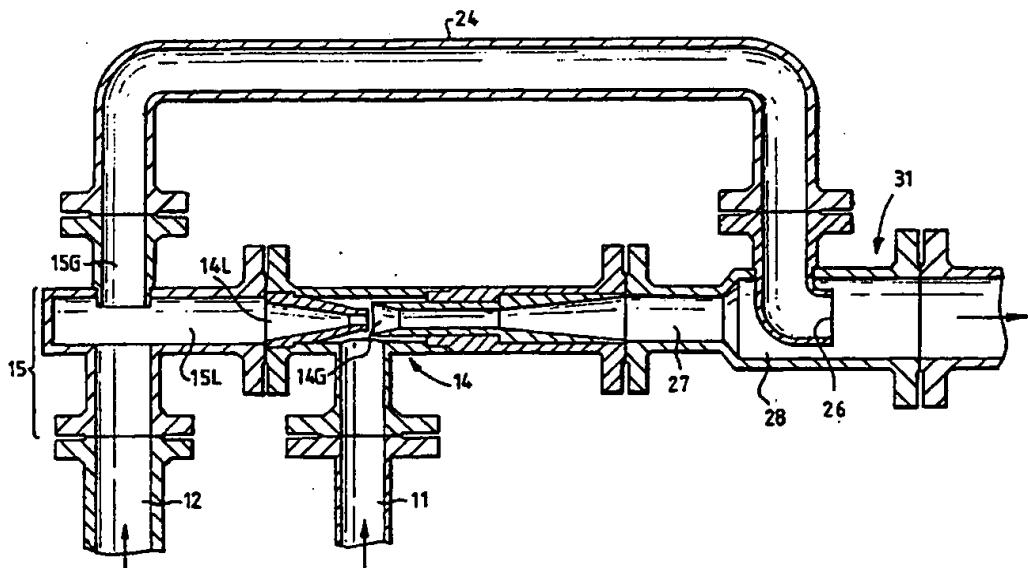


INTERNATIONAL APPLICATION PUBLISHED UNDER THE PATENT COOPERATION TREATY (PCT)

(51) International Patent Classification 6 : F04F 5/10, E21B 43/12	A1	(11) International Publication Number: WO 95/07414 (43) International Publication Date: 16 March 1995 (16.03.95)
--	----	--

(21) International Application Number: PCT/GB94/01937	(81) Designated States: AU, BR, GB, JP, NO, US, European patent (AT, BE, CH, DE, DK, ES, FR, GB, GR, IE, IT, LU, MC, NL, PT, SE).
(22) International Filing Date: 6 September 1994 (06.09.94)	
(30) Priority Data: 9318419.0 6 September 1993 (06.09.93) GB	Published <i>With international search report. Before the expiration of the time limit for amending the claims and to be republished in the event of the receipt of amendments.</i>
(71) Applicant (for all designated States except US): B.H.R. GROUP LIMITED [GB/GB]; Cranfield, Bedford MK43 0AJ (GB).	
(72) Inventor; and	
(75) Inventor/Applicant (for US only): SARSHAR, Mir, Mahmood [GB/GB]; 2 Woodside Avenue, Beaconsfield, Bucks HP9 1JL (GB).	
(74) Agent: CLINE, Roger, Ledlie; Edward Evans & Co., Chancery House, 53-64 Chancery Lane, London WC2A 1SD (GB).	

(54) Title: SYSTEM FOR PUMPING LIQUIDS USING A JET PUMP



(57) Abstract

A co-mingling device comprises a jet pump (14) and a phase separator (15). The jet pump has a primary fluid which is a driving fluid and a secondary fluid which is the driven fluid. It is particularly important that the primary fluid is consistent in phase, and to avoid undue phase variations, the present invention includes the phase separator (15) in the primary fluid supply, directing liquid-rich fluid (15L) to the primary fluid input (14L) of the jet pump. The gas-rich fluid 15G can bypass the jet pump in (24) and be mingled at (28) with the output of the jet pump if desired.

FOR THE PURPOSES OF INFORMATION ONLY

Codes used to identify States party to the PCT on the front pages of pamphlets publishing international applications under the PCT.

AT	Austria	GB	United Kingdom	MR	Mauritania
AU	Australia	GE	Georgia	MW	Malawi
BB	Barbados	GN	Guinea	NE	Niger
BE	Belgium	GR	Greece	NL	Netherlands
BF	Burkina Faso	HU	Hungary	NO	Norway
BG	Bulgaria	IE	Ireland	NZ	New Zealand
BJ	Benin	IT	Italy	PL	Poland
BR	Brazil	JP	Japan	PT	Portugal
BY	Belarus	KE	Kenya	RO	Romania
CA	Canada	KG	Kyrgyzstan	RU	Russian Federation
CF	Central African Republic	KP	Democratic People's Republic of Korea	SD	Sudan
CG	Congo	KR	Republic of Korea	SE	Sweden
CH	Switzerland	KZ	Kazakhstan	SI	Slovenia
CI	Côte d'Ivoire	LI	Liechtenstein	SK	Slovakia
CM	Cameroon	LK	Sri Lanka	SN	Senegal
CN	China	LU	Luxembourg	TD	Chad
CS	Czechoslovakia	LV	Latvia	TG	Togo
CZ	Czech Republic	MC	Monaco	TJ	Tajikistan
DE	Germany	MD	Republic of Moldova	TT	Trinidad and Tobago
DK	Denmark	MG	Madagascar	UA	Ukraine
ES	Spain	ML	Mali	US	United States of America
FI	Finland	MN	Mongolia	UZ	Uzbekistan
FR	France			VN	Viet Nam
GA	Gabon				

SYSTEM FOR PUMPING LIQUIDS USING A JET PUMP

Jet pumps operate by introducing a high pressure or primary fluid through a nozzle and allowing the low pressure or secondary fluid to be entrained into the flow stream. Due to the momentum exchange between the two fluids the resulting pressure of the combined stream will be increased to well above the pressure of the secondary fluid.

An application of mingling liquids is in fuel extraction. Gas or liquid or a mixture of the two phases is extracted from a fuel field. Many fields have a significant variation in production characteristics because of reservoir fragmentation and presence of different production zones. This often results in wells having different flowing wellhead pressures.

Conventional mingling of the products from such wells results in the need to choke the production from the high pressure wells and restricts the production from the low pressure wells. This is costly and inefficient and does not result in optimum recovery.

Jet pumps can be used for such mingling and work satisfactorily when the primary and secondary fluids are both liquids, or both gases. In addition, jet pumps can also be designed to operate satisfactorily when the primary fluid is pure liquid and the secondary fluid consists of a liquid/gas mixture. However satisfactory, jet pump operation cannot be achieved when there is a wide variation in the phase proportions in the primary fluid.

The present invention is aimed at overcoming this problem by providing a co-mingling device in which the jet pump is provided with a phase separator in the primary line, and utilising the liquid phase obtained from the

separator as the primary fluid of the jet pump. A bypass arrangement may be provided for the separated gas phase to be mixed back into the fluids from the outlet of the jet pump.

5 Examples of the invention will now be described with reference to the accompanying drawings in which:-

Figure 1 is a diagrammatic representation of a co-mingling device,

Figure 2 is a diagram of the device of Figure 1,

10 Figure 3 is a diagram of a similar co-mingling system, incorporating two jet pumps,

Figure 4 shows a co-mingling system which is also a separating system, co-mingling the separated fluids, and

Figure 5 is an elaboration of Figure 4.

15 In Figures 1 and 2, fluids from separate sources are co-mingled in a jet pump 14. Sources of high and low pressure fluids for the jet pump are obtained in this example from underground oil wells, a first source of fluid 11 under low pressure and a second source of fluid 12 under 20 high pressure. Both fluids are mixtures of gas and liquid. The fluid from the high pressure oil well is used to pump fluid from the low pressure well.

The fluid mixture under low pressure is supplied to the low pressure inlet 14G of a conventional jet pump 14.

25 The high pressure fluid passes first to an in-line separator 15, in which the lighter phase tends to return to the line of entry and the heavier fluids are deflected from that line. This is usually achieved by imparting a swirl to the incoming fluid, the centrifugal force acting to 30 separate the different phases. The gas rich fluid tends to collect along the axis of the swirl, in line with the incoming fluid and the heavier phase is collected from an off-axis outlet.

The liquid phase (or liquid rich fluid) 15L separated from the high pressure fluid is supplied as primary fluid to the high pressure inlet 14L of the jet pump 14. The gas-rich phase 15G separated from the high pressure fluid 5 passes through a bypass conduit 24, and the conduit may be provided with a device for controlling the flow of the gas in the bypass conduit; the device may be an orifice plate, a nozzle (as illustrated at 26) at the end of the bypass conduit 24 or a controllable valve, which is useful when 10 inlet pressures may vary during operation.

Since the primary fluid reaching the high pressure inlet 14L of the jet pump is substantially all liquid phase, the jet pump 14 operates satisfactorily to draw low pressure fluid from the first source through the pump and 15 the mixture of liquids passes from the jet pump outlet 27, into a mixing device 28 where it is mixed with the gas stream from the separator 15.

It will be noted that the mixing device 28 is housed in an extension of the outlet pipe 31 of the jet pump; the 20 diameter of the extension increases in the region of the entry of the gas bypass conduit outlet. The role of the mixing device is to allow efficient entry of the bypass gas into the fluid leaving the jet pump. Since the pressure of the two fluids may be comparable at this point the mixing 25 device must reduce the effect which the high pressure bypass gas may have in restricting the flow out of the jet pump. In fact the bypass gas is probably at a higher pressure than the fluids in the outlet of the jet pump and so it is preferable for the outlet of the bypass conduit to 30 form what can be seen as another jet pump in the outlet conduit from the main jet pump, thus assisting the flow of fluids from the main jet pump, recovering momentum lost from the high pressure oil stream at the phase separator. Certainly the bypass gases should be introduced in a 35 streamline manner, such as by directing the gases axially

along the outlet conduit, to prevent any disruption of the flow from the outlet of the main jet pump. The effect of the outlet fluids from the main jet pump on the flow of gas in the bypass conduit controls the operation of the phase 5 separator; its back pressure discourages any carry-over of liquid slugs through the bypass conduit; it is thus a passive controller.

The gas from the separator 15 need not be mixed back with the output fluids from the jet pump. The gas may for 10 example be fed to a flare or a fuel system.

In Figure 3 there are two jet pumps 31, 32 in parallel and two phase separators 41, 42, one in the supply from each well. The first jet pump 31 receives liquid at each of its inputs, the liquid phase output 41L from the 15 high pressure well separator 41 as its primary fluid and the liquid phase output 42L from the low pressure well separator 42 as its secondary input, co-mingling them to produce a liquid supply 43L to the single mixing device 43. The second pump 32 receives gas-rich fluid at each of its 20 inputs, the gas phase output 41G from the high pressure well separator 41 as its primary fluid and the gas phase output 42G from the low pressure well separator 42 as its secondary fluid, comingling the gases to produce a gas supply 43G to a single mixing device 43. Jet pumps 25 receiving the same phase for primary and secondary fluids have improved performance, as was pointed out in the introduction to the specification.

The jet pump 14 in Figures 1 and 2 has a liquid enriched supply of driving fluid, but the supply from the low 30 pressure well is unseparated and so may contain unsatisfactory amount of gas. In Figure 3 both jet pumps 31, 32 have phase separated supplies and so do not have to deal with such a wide range of phase proportions; they can

therefore be much more closely designed and so should work more efficiently.

It would be possible for the high pressure inlet of the jet pump to be supplied from the liquid rich output of the 5 phase separator boosted in pressure for example by a pump and for the low pressure input of the jet pump to be supplied from the gas rich outlet of the phase separator. As shown in Figure 4, there is only one phase separator 51 and one manifold inlet 52 from an oil field. The jet pump 10 53 receives fluid at 53L from the liquid rich outlet 51L of the separator 51 after boosting in pressure by a pump 55. The gas rich outlet 51G of the separator is not boosted and so is at relatively low pressure at the low pressure inlet 53G to the jet pump. The jet pump has a narrow range of 15 phase proportions to deal with as its primary fluid and operates efficiently to co-mingle the gas and liquid phases from the oil field.

Figure 4 shows the arrangement of Figure 3 with the output from a second manifold 61 of fluids at higher pressures. 20 The second manifold is connected to the output 56 of the jet pump 53 by a further co-mingler 62, which may be another jet pump or a general mixing device, as described above.

CLAIMS

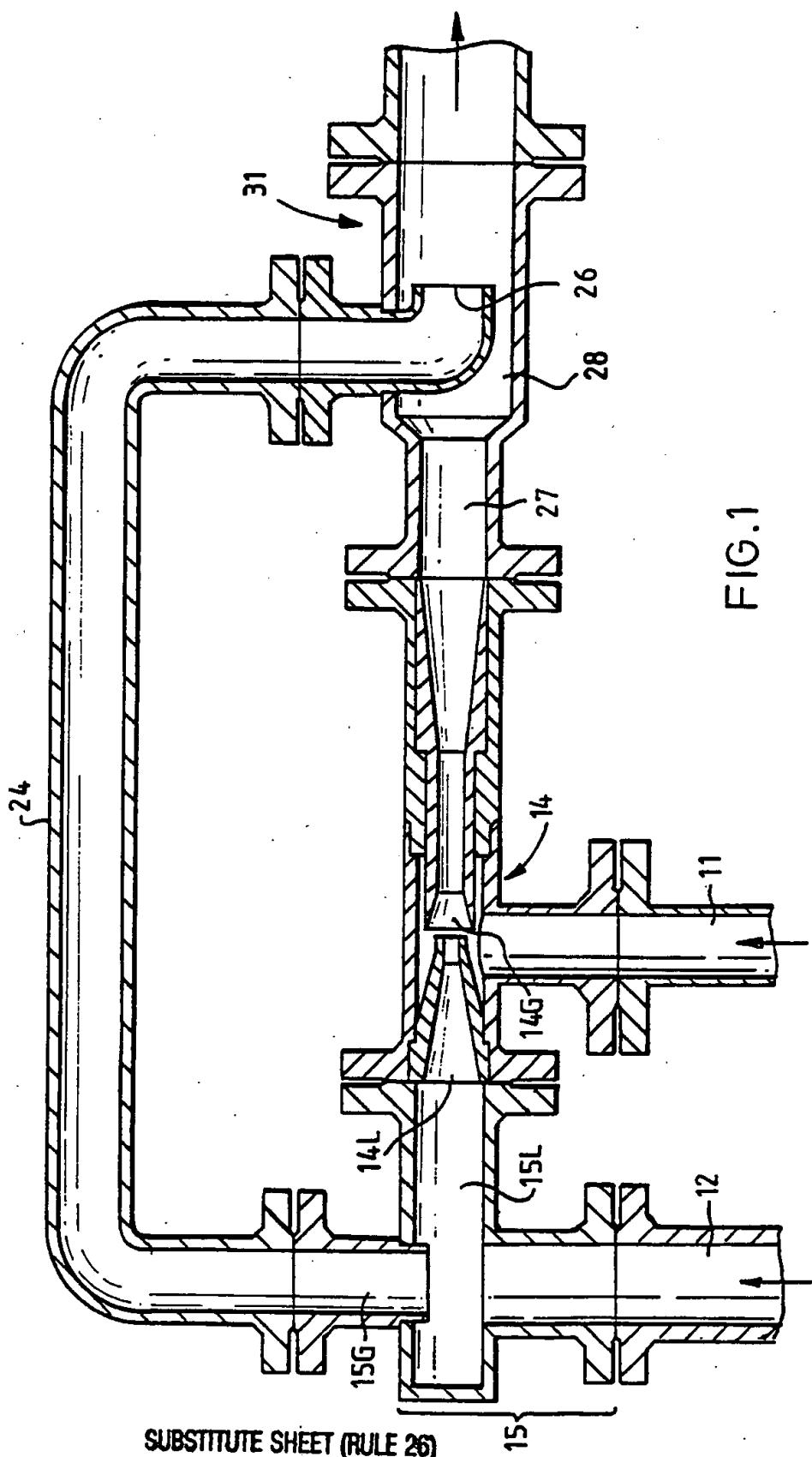
1. A co-mingling device comprising a jet pump (14, 32, 53) having a high pressure inlet (14L, 32L, 53L), a low pressure inlet (14G, 32G, 53G) and a main outlet (27, 43L, 56), characterised by a phase separator (15, 42, 51) having a liquid-rich outlet (15L, 42L, 51L) connected to said high pressure inlet.
2. A device as claimed in claim 1 wherein the phase separator has a gas-rich outlet (14G, 32G, 53L) which is connected to said main outlet.
3. A device as claimed in claim 2 wherein the gas-rich outlet is connected to said main outlet by means of a nozzle (26) directed along the axis of the main outlet.
4. A device as claimed in claim 1 wherein the phase separator has a gas rich outlet (51G) which is connected to said low pressure inlet (53G), means (55) being provided between the liquid rich outlet (51L) and the high pressure inlet (53L) to increase the pressure of fluid passing therethrough.
5. A co-mingling device as claimed in claim 1 where said jet pump is a first jet pump (31) having a high pressure inlet, a low pressure inlet and a main outlet, and said phase separator is a first phase separator (41) having a liquid-rich outlet connected to said high pressure inlet of the first jet pump, the device comprising a second jet pump (32) having a high pressure inlet, a low pressure inlet and a main outlet, and a second phase separator (42) having a liquid-rich outlet connected to said low pressure inlet of the first jet pump, the first phase separator having a gas rich outlet connected to the high pressure inlet of the second jet pump and the second gas separator having a gas

rich outlet connected to the low pressure inlet of the second jet pump.

6. A device as claimed in claim 5 comprising means (43) to mix the outlets of the two jet pumps (31, 32).

5 7. A device as claimed in any one of claims 1 to 6 wherein the or each phase separator is an in-line separator, the gas-rich outlet (15G, 41G, 51G) being aligned with the inlet of the phase separator.

1/3



2/3

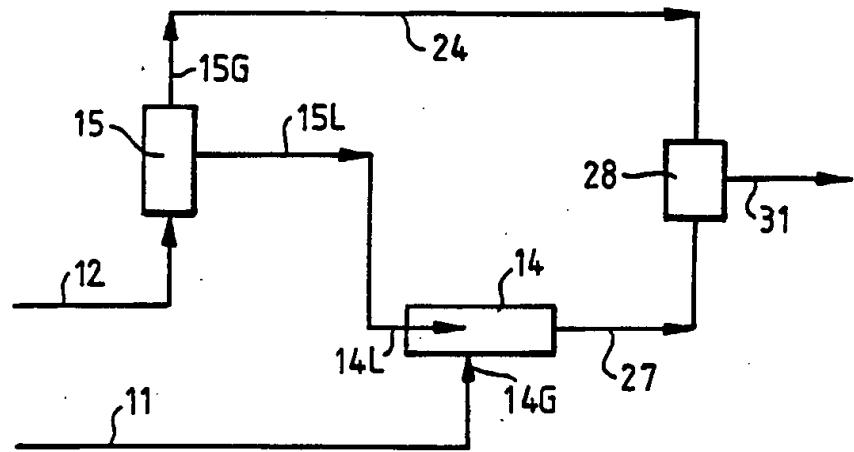


FIG. 2

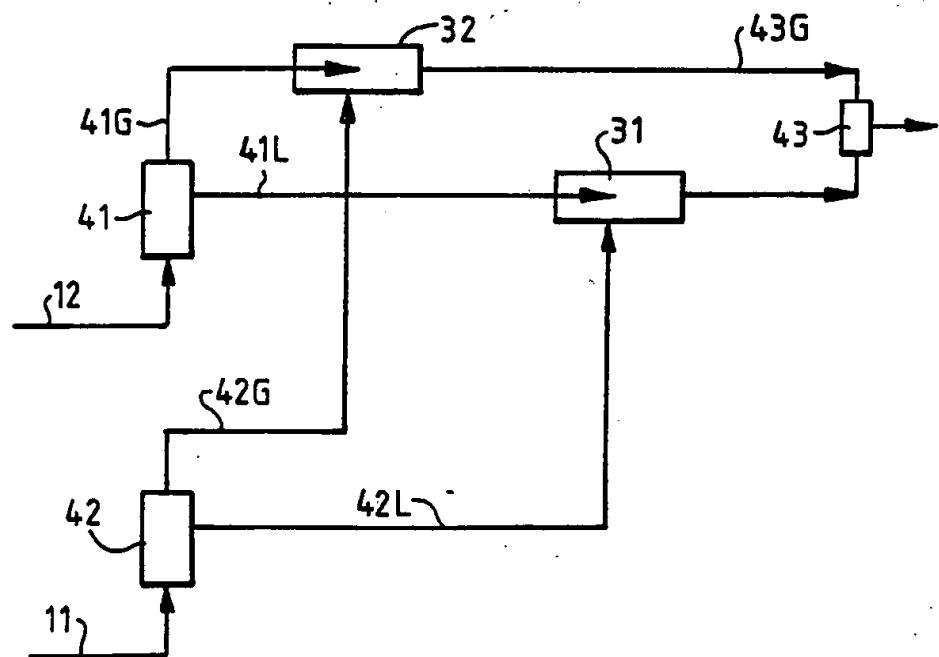


FIG. 3

3/3

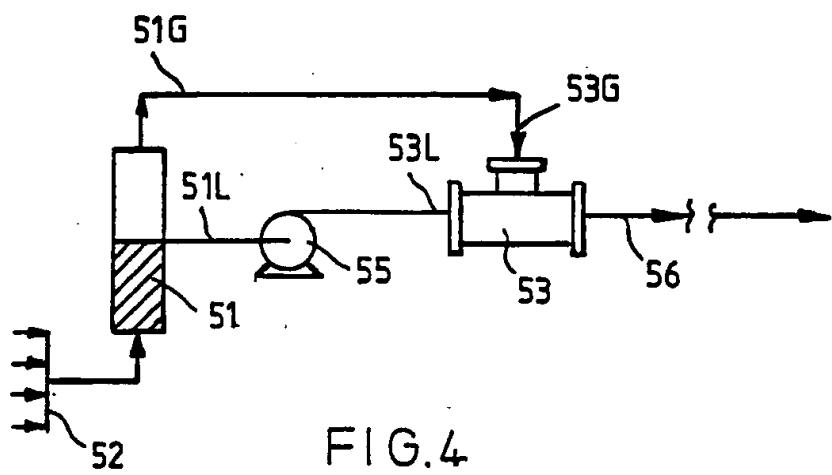


FIG. 4

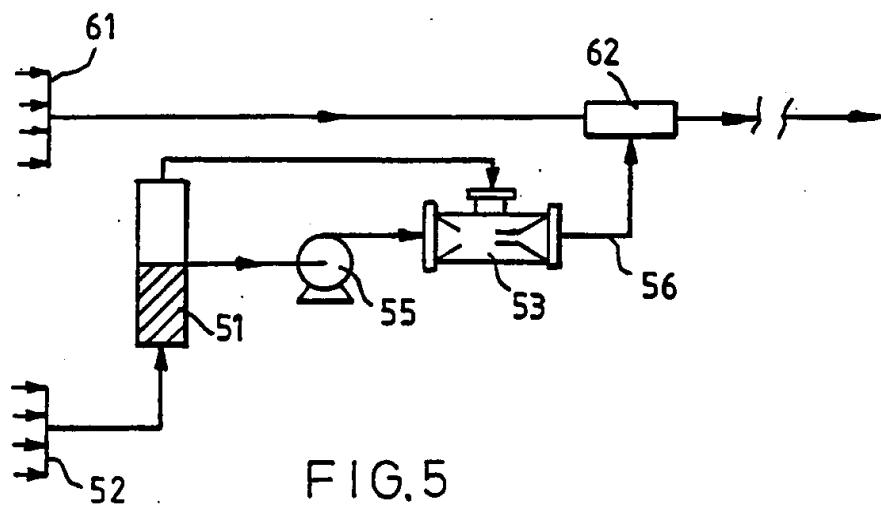


FIG. 5

INTERNATIONAL SEARCH REPORT

Intern al Application No
PCT/GB 94/01937A. CLASSIFICATION OF SUBJECT MATTER
IPC 6 F04F5/10 E21B43/12

According to International Patent Classification (IPC) or to both national classification and IPC

B. FIELDS SEARCHED

Minimum documentation searched (classification system followed by classification symbols)
IPC 6 F04F E21B F04D

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Electronic data base consulted during the international search (name of data base and, where practical, search terms used)

WPI, PAJ, Compendex, Apilit, Ismec, Dialog Sourceone

C. DOCUMENTS CONSIDERED TO BE RELEVANT

Category	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
X	GB,A,2 264 147 (PECO MACHINE SHOP & INSPECTION SERVICES LTD.) 18 August 1993 see page 7, line 14 - line 32; figure 3	1
A	GB,A,2 239 676 (B.H.R. GROUP LTD.) 10 July 1991 see page 1, line 18 - line 26; figure 1	1
A	GB,A,2 101 216 (THE PLESSEY COMP.) 12 January 1983 see page 1, line 86 - line 99; figures 1,6	1

 Further documents are listed in the continuation of box C. Patent family members are listed in annex.

* Special categories of cited documents :

- *A* document defining the general state of the art which is not considered to be of particular relevance
- *E* earlier document but published on or after the international filing date
- *L* document which may throw doubts on priority claim(s) or which is cited to establish the publication date of another citation or other special reason (as specified)
- *O* document referring to an oral disclosure, use, exhibition or other means
- *P* document published prior to the international filing date but later than the priority date claimed

- *T* later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention
- *X* document of particular relevance; the claimed invention cannot be considered novel or cannot be considered to involve an inventive step when the document is taken alone
- *Y* document of particular relevance; the claimed invention cannot be considered to involve an inventive step when the document is combined with one or more other such documents, such combination being obvious to a person skilled in the art.
- *&* document member of the same patent family

Date of the actual completion of the international search

6 January 1995

Date of mailing of the international search report

12.01.95

Name and mailing address of the ISA

European Patent Office, P.B. 5818 Patentlaan 2
NL - 2280 HV Rijswijk
Tel. (+31-70) 340-2040, Tx. 31 651 epo nl,
Fax (+31-70) 340-3016

Authorized officer

Rampelmann, K

INTERNATIONAL SEARCH REPORT

Intern. Application No
PCT/GB 94/01937

Patent document cited in search report	Publication date	Patent family member(s)		Publication date
GB-A-2264147	18-08-93	NONE		
GB-A-2239676	10-07-91	NONE		
GB-A-2101216	12-01-83	DE-A,C FR-A,B US-A-	3221231 2508558 4461678	13-01-83 31-12-82 24-07-84